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In re: Patent application of :  
Ian Fraser Jarvies, *et al.* :  
Serial No.: 10/523,497 : Group Art Unit:  
1724  
Filed: February 4, 2005 : Examiner:  
Not Yet Assigned  
For: APPARATUS AND METHOD FOR :  
TREATMENT OF CHEMICAL AND BIOLOGICAL : Conf. No. 1844  
HAZARDS

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Respectfully submitted,

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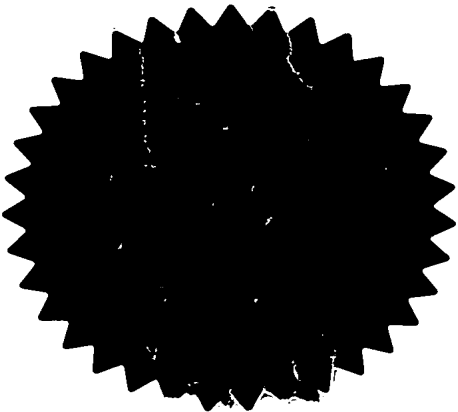
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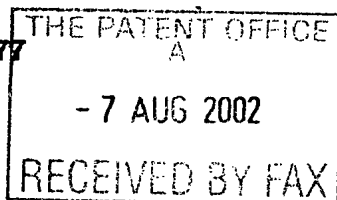


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3. 1

0218314.3

each applicant (*underline all surnames*)Albagia Limited  
Adziel House  
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Aberdeenshire AB43 6TBPatents ADP number (*if you know it*)

If the applicant is a corporate body, give the country/state of its incorporation

UK

8441899001

4. Title of the invention

Apparatus and Method for Treatment of Chemical and Biological Hazards

5. Name of your agent (*if you have one*)

Murgitroyd &amp; Company

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**Patents Form 1/77**

1 APPARATUS AND METHOD FOR TREATMENT OF CHEMICAL AND  
2 BIOLOGICAL HAZARDS

3  
4 The present invention relates to an apparatus for the  
5 treatment of hazardous materials specifically prions,  
6 chemical and biological agents. The invention further  
7 relates to a method for using such an apparatus.

8  
9 The risks associated with contamination caused by  
10 chemical and biological agents of various kinds are  
11 well known. Medical equipment and surgical instruments  
12 are required to be sterilised to eliminate a growing  
13 range of infectious agents including more recently  
14 prions implicated in new variant Creusfeld Jacob  
15 Disease (nvCJD). Proteins exhibit huge variation in  
16 structure. However, they are formed in similar ways  
17 and thus display certain structural elements and  
18 characteristics that are common. The primary structure  
19 of proteins is determined by the amino acid sequence  
20 and pendant side groups. The amino acid chains are  
21 then folded to form various secondary structures

1 designated as  $\alpha$ -helices or  $\beta$ -sheets. Secondary  
2 structure is determined by the folding of the amino  
3 acid chains and interactions between the various side  
4 groups. Further associations may also form, depending  
5 on the protein's environment. For example different  
6 hydrophilic and hydrophobic groups or areas within the  
7 protein molecule are sensitive to the medium in which  
8 the molecule may be suspended. The prion protein plays  
9 an essential role in the pathogenesis of a group of  
10 sporadic, genetically determined and infectious fatal  
11 degenerative diseases, referred to as prion diseases,  
12 or transmissible encephalopathys (TSE's), affecting the  
13 central nervous system of humans and other mammals.  
14 The cellular prion protein is encoded with a single  
15 copy gene, highly conserved across mammalian species.  
16 In prion diseases this protein undergoes conformational  
17 changes involving a shift from  $\alpha$ -helix to  $\beta$ -sheet  
18 structure. The structures of the proteins, both native  
19 and rogue, have been extensively investigated. The one  
20 of most interest and immediate impact to humans is the  
21 protein associated with nvCJD. What is unusual about  
22 the protein that is associated with TSEs is the extreme  
23 robustness it exhibits. This is thought to be due its  
24  $\beta$ -sheet structure. Prions are known to survive  
25 temperatures in excess of 300 °C. Such proteins thus  
26 represent present particular problems in terms of their  
27 transmission and destruction. The nvCJD prion is known  
28 to have a high affinity for stainless steel and other

1 metals posing significant difficulties for the  
2 sterilisation of medical equipment, such as surgical  
3 instruments. At the same time, considering hazards  
4 unrelated to the medical field, chemical and biological  
5 agents, such as those used as weapon materials, pose  
6 significant handling and disposal risks.

7

8 For the purposes of the present application, the term  
9 "hazardous material" means any organic material that  
10 may be inimical to human well being and as such may be  
11 classed as a chemical or biological hazard. "Hazardous  
12 material" includes, but is not restricted to, viral  
13 material, bacterial material, prions, proteins, lipids,  
14 chemical and biological agents / material with  
15 associated organophosphate bases, organic waste or by-  
16 products associated with pharmaceutical processes and  
17 blood products, and further includes all of said agents  
18 in isolation and when found within, on the surface of  
19 or bonded to other material, instruments or equipment.  
20 The term "target material" is used throughout in  
21 reference to a "hazardous material" which is to be  
22 treated according to the method of the invention.

23

24 The term "treatment" is used in its broadest form and  
25 encompasses the deactivation and destruction of  
26 hazardous material. Relatively minor modifications to  
27 the structure or conformation of a particular agent may  
28 be sufficient to render it inactive without the need



1 for the agent to be destroyed or decomposed into  
2 constituent elements.

3

4 While some methods for treating such agents are known,  
5 these typically involve the use of reagents which are  
6 themselves difficult to handle and which have  
7 associated safety issues. Fluorine and ozone for  
8 example may be effective in catalysing such processes,  
9 but create significant handling problems and are not  
10 suited to use in an open bath apparatus. Furthermore  
11 some prior art processes are required to be carried out  
12 at very high temperatures and / or pressures. The  
13 apparatus used in such processes is necessarily complex  
14 and expensive in light of the associated handling  
15 difficulties.

16

17 There remains therefore a need for a method for the  
18 deactivation or destruction of prions, chemical and  
19 biological agents, which is effective, efficient and  
20 broadly applicable. There is a particular need for an  
21 apparatus and a treatment method that can be used to  
22 sterilise or decontaminate equipment and instruments  
23 that may have come into contact with hazardous  
24 material. The present invention as set out below  
25 provides such an apparatus and a method for its use.

26

27 Accordingly, in a first aspect the present invention  
28 provides apparatus for treating hazardous material and  
29 for decontaminating items that may have come into

1 contact with such material. In its broadest form such  
2 apparatus comprises an operator accessible treatment  
3 vessel or chamber and a light source capable of  
4 irradiating a catalyst within the treatment vessel or  
5 chamber with a predetermined wavelength.

6

7 A first embodiment of the invention provides an  
8 apparatus, for batch treatment of hazardous material,  
9 comprising a treatment vessel for holding material to  
10 be treated; a light source for irradiating the contents  
11 of the treatment vessel; circulation or agitation means  
12 and progress and / or by-product monitoring means. The  
13 treatment vessel may comprise a 'glove box' type lid  
14 facilitating manipulation of the bath contents by an  
15 operator. An automatic light source cut-off may be  
16 incorporated in order to enhance operator safety.

17

18 A second embodiment provides an apparatus comprising a  
19 treatment vessel having one or more decontamination  
20 trays for holding hazardous material or items to be  
21 treated, a light source for irradiating the contents of  
22 the treatment vessel, medium distribution means for  
23 circulating a carrier medium within and / or through  
24 the apparatus and by-product monitoring means.

25

26 A third embodiment provides an apparatus comprising a  
27 holding tank for holding a carrier medium; a catalyst  
28 hopper for holding a catalyst; a mixing vessel for  
29 mixing the carrier medium and the catalyst; one or more

1 treatment chambers each having a housing which contains  
2 a plurality of treatment beds and a light source; and a  
3 distribution header for controlling the flow of carrier  
4 medium and catalyst into the treatment chambers.  
5 Preferably, each treatment bed comprises means for  
6 inducing turbulent flow within the carrier medium  
7 flowing therein.

8

9 A second aspect of the present invention provides a  
10 method for the deactivation and / or destruction of  
11 hazardous material comprising the step of irradiating  
12 the hazardous material in the presence of a catalyst  
13 with light having a wavelength in the range of 310 nm  
14 to 400 nm. The method of the invention causes  
15 sufficient chemical modification of the hazardous  
16 material so as to deactivate or destroy it.

17

18 Preferably, the catalyst is  $\text{TiO}_2$  in either rutile or  
19 anatase form and preferably the method is carried out  
20 at ambient temperature (of between about 15 to 35 °C)  
21 and pressure (of between about 1 to 5 bar).

22

23 The method may be carried out in any water based  
24 carrier medium that is compatible with the target  
25 material and catalyst. Preferably the carrier medium  
26 is water. Judicious choice of treatment medium is  
27 required in order to ensure reliable and effective  
28 treatment. In particular when considering the  
29 treatment of objects or instruments contaminated with

1 prions for example the physical characteristics of the  
2 apparatus and method should facilitate a suitable  
3 reaction interface. This involves consideration of the  
4 composition and viscosity of the carrier medium and the  
5 path-length of the apparatus such that the target  
6 material, catalyst and photons from the light source  
7 are brought together in a manner suitable to effect  
8 treatment. It follows that a medium that is relatively  
9 low in viscosity and has appropriate optical  
10 characteristics (over the wavelength(s) of the light  
11 source) is desirable. In other words, the viscosity  
12 must be such as to allow the bringing together of the  
13 target material and the catalyst and the configuration  
14 of the apparatus and the optical characteristics of the  
15 medium must allow sufficient transmission of light to  
16 the target / catalyst reaction site.

17

18 Thus, the present invention provides for the treatment  
19 hazardous material such as prions linked with human or  
20 animal nvCJD in both  $\alpha$  and  $\beta$  forms and for treatment of  
21 instruments and equipment that may have been  
22 contaminated with said material. The method, and  
23 apparatus for implementing it, are also applicable to  
24 the destruction of chemical agent material, typically  
25 organophosphate based systems, as typified by VX or  
26 Sarin, but additionally blistering and choking agents  
27 as typified by Mustard Gas and Tear Gas. Depending  
28 upon the conditions employed, the invention provides

1 for total destruction of some hazardous material by  
2 breaking it down into its constituent parts,  
3 principally carbon dioxide, nitrogen, water and  
4 inorganic salts, or alternatively provides for  
5 sufficient modification of target materials so as to  
6 render them inactive. The invention can also  
7 deactivate or destroy many other biohazards, viral and  
8 bacteriological material, and many commonly  
9 industrially produced organic materials. Furthermore,  
10 the method of the invention can be employed to  
11 decontaminate materials, equipment, instruments and the  
12 like which may have come into contact with hazardous  
13 material.

14

15 The method of the invention represents an efficient  
16 means of deactivating and / or destroying of hazardous  
17 material under mild conditions on a batch basis.  
18 Further advantages of the invention are described  
19 below.

20

21 The various aspects of the invention are described in  
22 detail below with reference to the accompanying  
23 drawings in which:

24

25 Figure 1 shows a first embodiment of an apparatus  
26 according to the invention;  
27 Figure 2 shows a second embodiment of an apparatus  
28 according to the invention;

1 Figure 3 shows a third embodiment of an apparatus  
2 according to the invention; and  
3 Figures 4 and 5 are more detailed views of the  
4 treatment chamber of the embodiment shown in Figure 3.

5  
6 In the drawings similar reference numerals have been  
7 used to designate components common to each of the  
8 alternative embodiments.

9  
10 In its broadest form the invention provides a  
11 decontamination method for the treatment of hazardous  
12 material comprising the step of irradiating the  
13 hazardous material in the presence of a catalyst, with  
14 light of a suitable wavelength, to deactivate or  
15 destroy the target material through photocatalytic  
16 oxidative processes. In general terms, the apparatus  
17 of the present invention comprises (i) a treatment  
18 chamber in which the catalyst and the target material  
19 may be irradiated with light of a suitable wavelength  
20 (and energy) and (ii) a light source capable of  
21 producing the desired wavelength. The light source  
22 wavelength and intensity may be adjusted to optimise  
23 the process depending upon the nature of the target  
24 material and the choice of catalyst. A liquid carrier,  
25 preferably a water based medium, is used to introduce  
26 hazardous material into the treatment chamber for  
27 irradiation.

28

1 Without being bound by theory, the invention is  
2 considered to be the result of an interaction of light  
3 energy (photons), the catalyst and water elements that  
4 forms hydroxyl radicals which cleave sections of, or  
5 links in, molecules of the target material ('primary  
6 effects'). The action of UV light contributes directly  
7 to the breakdown of target materials through photolysis  
8 of molecules present. In conjunction with the  
9 formation of hydroxyl radicals hydrogen peroxide ( $H_2O_2$ )  
10 is also produced. This oxidising agent assists and  
11 speeds the decontamination process cycle. The primary  
12 effects of hydroxyl radicals allow secondary processes  
13 (such as attack by  $H_2O_2$ ) to act upon vulnerable parts of  
14 the molecules. The ultimate result is the break down  
15 of hazardous material into simple (safe) moieties,  
16 formation of inorganic salts within the carrier medium  
17 and production of off-gases, such as  $CO_2$ .

18  
19 The method of the invention employing highly reactive  
20 hydroxyl radicals and  $H_2O_2$  produced through irradiation  
21 of a suitable catalyst can be utilised to oxidise prion  
22 proteins decomposing them to  $NO_x$ ,  $CO_2$ , water and various  
23 inorganic salts. Attack on a prion protein molecule by  
24 a hydroxyl radical causes selective breakage of  
25 multiple bond linkages, thus permanently altering the  
26 crucial relationship between amino acid units and  
27 inducing changes to their proper attachment and  
28 alignment to each other (and to associated components  
29 such as carbohydrates and possibly lipids). This

1 effect changes the spatial configuration of the prion  
2 protein impacting upon its ability to reproduce  
3 properly. It is possible that even small alterations  
4 in the protein composition and / or configuration are  
5 sufficient to impede biological activity of a prion  
6 molecule. Any alteration in the structural make-up and  
7 configuration reduces the resistance of the prion to  
8 further oxidative processes, such as attack by  $H_2O_2$ ,  
9 thus increasing the rate of complete oxidation of the  
10 molecule.

11

12 Contact between the hydroxyl radical / hydrogen  
13 peroxide production interface and the target material  
14 on the equipment / instruments or the like, using the  
15 water based carrier medium with the catalyst, should be  
16 maximised. This may be addressed by ensuring that the  
17 catalyst within the water carrier is migrated to the  
18 interface using suitable circulation or entraining  
19 processes. Minimising the spatial offset in this  
20 manner increases the effects of the short-lived  
21 radicals produced upon irradiation.

22

23 Increasing the intensity of irradiation and / or  
24 increasing the surface area of catalyst irradiated can  
25 increase radical production. Additional catalyst may  
26 be introduced to speed the process and replace catalyst  
27 extracted from the waste stream.



1 The catalyst may be any photosensitive material, which  
2 allows, through illumination with light of a suitable  
3 wavelength, a reaction with the associated hazardous  
4 material to occur. Suitable catalyst materials include  
5 for example  $\text{TiO}_2$ ,  $\text{TiO}_3$ ,  $\text{ZnO}$ ,  $\text{CdS}$ ,  $\text{CdSe}$ ,  $\text{SnO}_2$ ,  $\text{WO}_3$ ,  $\text{Fe}_2\text{O}_3$   
6 and  $\text{Ta}_2\text{O}_5$ . An example of a preferred catalyst is  $\text{TiO}_2$ .  
7 Irradiation of the catalyst produces active sites (on  
8 what is in effect a semiconductor surface) causing  
9 water absorbed to the surface to be oxidised. Highly  
10 reactive hydroxyl radicals formed in this manner react  
11 with (and ultimately decompose) the target material  
12 present in the system.

13  
14 The catalyst may be used in any form that provides  
15 suitable contact with the target material. For  
16 example, the catalyst may be dispersed in the carrier  
17 medium or it may be coated onto or mixed with the  
18 various materials to be decontaminated or destroyed. A  
19 catalyst module such as a column or tower coated with  
20 catalyst material may be employed. Alternatively, the  
21 catalyst may be coated onto internal surfaces of the  
22 apparatus, enhancing robustness and self-cleaning  
23 capability. Recovery of the catalytic material for  
24 reuse, increasing efficiency of the process, may be  
25 provided for as described below.

26  
27 While light in the range of 310 nm to 400 nm is  
28 preferred, the wavelength of light employed may vary  
29 depending upon the catalyst used, the medium used and

1 the nature of the target material. The wavelength to  
2 be used may be selected based on the absorption  
3 characteristics of the target material, thus increasing  
4 efficiency. As photo-generated hydroxyl radicals are  
5 the primary agents responsible for the decontamination  
6 / destruction processes various parameters may be  
7 changed to optimise the effect upon any given target  
8 material. The selected wavelength may be produced for  
9 example using a standard mercury lamp in conjunction  
10 with a suitable filter.

11

12 The method of the invention degrades target materials  
13 ultimately reducing them to simple reaction products  
14 such as  $\text{CO}_2$ . The evolution of  $\text{CO}_2$  or any other reaction  
15 product can thus be used to monitor the degree and rate  
16 of the process. Suitably off-gas production or target  
17 material break down may be monitored using techniques  
18 such as Raman spectroscopy, mass spectrometry, in vitro  
19 tests or other known techniques appropriate to any  
20 particular hazardous material.

21

22 Characteristics of the method of the invention are  
23 detailed in Table 1, together with comparable data for  
24 various prior art methods. The 'efficiency' values  
25 indicate the rate and effectiveness of electron  
26 transfer during the treatment process.

Catalyst	Efficiency (eV)	Medium	Output toxicity	Temp (°C)	Pressure (bar)	Power
TiO <sub>2</sub> (present invention)	3.34	Water	Very low	<36	<10	Low
Ag (II)*	1.98	Nitric acid	High	~90	10	High
Ruthenium*	1.8	H <sub>2</sub> SO <sub>4</sub>	High	~90	10	High
Chlorination*	1.3	Water	High	~40	<10	Low
H <sub>2</sub> O <sub>2</sub> **	2.00	Water	Low	<36	<10	Low

1

2 Table 1.           \*Indicates prior art process; \*\*Hydrogen  
3                       peroxide not a catalyst as such - included  
4                       for comparison purposes only.

5

6 Prior art methods (other than those detailed in Table  
7 1) include hydrogenation and methods employing molten  
8 metals or supercritical water. These additional  
9 methods all pose significant hazards themselves due to  
10 the operating conditions required in order to be  
11 effective (for example, all three require temperatures  
12 in excess of 600 °C; and hydrogenation and  
13 supercritical water methods operate at pressures of  
14 about, or in excess of, 100 bar). Treatment with  
15 fluorine, possibly the strongest oxidising agent known,  
16 is also effective, but extremely difficult and  
17 dangerous to handle.

15

1 The method of the invention provides an effective and  
2 efficient process for the deactivation and / or  
3 destruction of hazardous material, on batch or  
4 continuous basis, while overcoming the shortcomings of  
5 some prior art methods in terms of operational  
6 requirements and characteristics. The present  
7 invention facilitates decontamination treatments to be  
8 carried out under ambient temperature and pressure  
9 conditions through a method and apparatus which has  
10 minimal moving parts, is easy to maintain and operate  
11 and which is readily scalable.

Class of Compound	Examples
Alkanes	Methane; pentane; heptane; n-dodecane; cyclohexane, paraffin
Haloalkanes	mono-, di-, tri-, and tetrachloromethane; dichloropropane Pentachloroethane; di and tribromoethane; 1,2-dichloropropane
Aliphatic Alcohols	methanol; ethanol; n- and iso-propanol; butanol; penta-1, 4-diol
Aliphatic Carboxylic Acids	methanoic, ethanoic; trichloroacetic; butyric; oxalic
Alkenes	propene; cyclohexene
Haloalkenes	di-, tri- and tetra-chloroethene; hexafluoropropene
Aromatics	benzene; naphthalene, Tributyl Phosphate
Haloaromatics	chloro and bromobenzene; chlorobenzenes; halophenols
Phenols	phenol; hydroquinone; catecol; resorcinol; cresol, nitrophenol
Aromatic Carboxylic Acids	benzoic; phthalic; salicylic
Polymers	polyethylene; PVC
Surfactants	polyethylene glycol; p-nonyl phenyl ether; sodium dodecyl benzene sulphonate; paraxon; malathion
Herbicides	methyl viologen; atrazine; simazine; bentazon
Pesticides	DDT; parathion; lindane, monocrotophos
Dyes	methylene blue; rhodamine B; methyl orange; fluorescein
Explosives	Trinitrotoluene
Cyanotoxins	Microcystins, Anatoxin-a
Bacteria	E.Coli., Serratia marcescens,
Proteins	

Table 2

1 Table 2 lists compounds successfully destroyed using  
2 the present invention. Tributyl phosphate, appearing  
3 in the 'Aromatics' class, is a simulant for nerve  
4 agents.

5

Material	Concentration (% v/v)	Wavelength (nm)	Time (min)	Efficiency (%)
Methanol	0.1	385 +/- 10	20	99.5
Paraffin	0.1	385 + / - 10	40	99.75
Benzene	0.1	380 + / - 10	60	99.9

6 Table 3.

7

8 Table 3 details a number of test materials and the  
9 conditions under which they were treated. In each case  
10 treatment was carried out at atmospheric pressure and  
11 at room temperature. The treatment efficiency (which  
12 in the case of the three test materials corresponds to  
13 destruction of the compounds in question) was measured  
14 using spectrophotometric techniques.

15

16 The specific embodiments of an apparatus according to  
17 the invention described below may each be provided with  
18 a circulation system, a catalyst feed mechanism, and a  
19 catalyst recovery system. In addition there may be a  
20 flushing mechanism to remove excess free catalyst  
21 deposits from the cleaned instruments or tools and  
22 materials prior to final removal and drying. Larger  
23 units having the same basic unit structure may be

1 complemented by material towers coated with the  
2 catalyst through which the contaminated material in the  
3 water-based matrix is allowed to percolate, thus  
4 increasing exposure of the contaminants to the catalyst  
5 and UV sources.

6  
7 A first embodiment of an apparatus according to the  
8 invention is shown schematically in Figure 1. The  
9 apparatus comprises a treatment chamber or bath (1), a  
10 light source (2), a circulation pump (3), an off-gas  
11 monitor / treatment unit (8), a catalyst recovery  
12 system (4) and a holding tank (5). A catalyst hopper  
13 (6) and a medium storage unit (7) for storing the  
14 catalyst and carrier medium prior to use are also  
15 provided. This first embodiment has been designed for  
16 small quantity throughput of, for example, surgical  
17 instruments for decontamination or for destruction of  
18 small quantities of target material. Manual  
19 manipulation of items in the treatment chamber may be  
20 facilitated through use of a glove-box type lid (9).  
21 This apparatus is designed for operation by medical  
22 staff in for example medical or dental practices.

23  
24 Catalyst material and carrier medium are introduced  
25 into the holding tank (5), from the catalyst hopper (6)  
26 and the medium storage unit (7) respectively, and from  
27 there into the treatment chamber (1). The catalyst is  
28 typically suspended in the carrier medium and suitable  
29 stirring means may be provided in order to ensure that

1 suspension is maintained and that the suspension  
2 circulates within the chamber (1). The contaminated  
3 equipment or target material (not shown) is placed in  
4 to the bath; the lid closed and interlocks (not shown)  
5 engaged before the process commences. In order to  
6 maintain the catalyst in suspension within the carrier  
7 medium during the process, the medium is circulated  
8 through the system by using suitable means. This  
9 facilitates maximum irradiation of the catalyst  
10 simultaneously allowing the catalyst particles to  
11 contact the interface with the target material. A  
12 circulating pump (3) is used for the removal of  
13 catalyst via the catalyst recovery system (4) at the  
14 end of the process run. The catalyst recovery system  
15 (4), typically takes the form of a cyclone separator.  
16 The level of catalyst in the system is monitored via  
17 the process controller (not shown) and adjusted to the  
18 required level. The carrier medium is circulated  
19 within the bath (1) during the  
20 decontamination/destruction process and may be replaced  
21 or replenished from the medium storage unit (7) or via  
22 the catalyst recovery system (4). The process  
23 controller (not shown) is used to monitor the overall  
24 process, including monitoring off-gas production within  
25 the off-gas monitor/treatment system (8). The off-gas  
26 monitoring system (8) provides the means by which the  
27 primary process status is monitored. The destruction  
28 of organic elements produces  $\text{CO}_2$ , when no further  $\text{CO}_2$   
29 production is detected the treatment process may be



1 regarded as complete. The residual CO<sub>2</sub> given off is  
2 collected by use of an active charcoal filter fitted  
3 into the off-gas system (8). Sampling can be  
4 facilitated in order to allow for conformity in vitro  
5 testing, spectroscopic analysis or the like to take  
6 place. Once completion of the process has been  
7 confirmed the used carrier medium can be disposed of in  
8 a recognised manner and the apparatus may be flushed  
9 with fresh medium. The flushing process enables all the  
10 areas within the apparatus that may have been  
11 contaminated by target material to be cleaned, although  
12 the system is inherently self-decontaminating. The  
13 carrier medium within treatment chamber (1) is then  
14 topped-up prior to next usage and the medium in the  
15 holding tank (7) replaced. While the method of the  
16 invention may generally be carried out at, or close to,  
17 atmospheric pressure, materials may be passed through  
18 the apparatus under higher pressure particularly during  
19 catalyst recovery and / or cleaning stages.

20  
21 Access to the treatment chamber (1) for this activity  
22 may be provided by a glove box lid arrangement (9).  
23 This allows for function (if necessary), dismantling  
24 and scrubbing of instruments or equipment to remove  
25 stubborn or hidden contaminants. These are  
26 subsequently circulated and destroyed in the treatment  
27 chamber during the treatment process. Safety  
28 interlocks may be employed to minimise any risks to  
29 personnel during operation, particularly when

21

1 introducing target material in to the apparatus.  
2 Switching means are provided for deactivating the light  
3 source automatically when the bath lid (9) is opened.

4

5 A second embodiment is shown schematically in Figure 2.  
6 This apparatus is designed for use in hospitals or  
7 larger clinics with high throughput of surgical  
8 instruments for decontamination. It is designed for  
9 operation by dedicated staff with training in the  
10 decontamination of surgical instruments and equipment.

11

12 The apparatus comprises a treatment chamber (1) having  
13 decontamination trays (10) an ultraviolet light source  
14 (2) and a medium distribution system (11). Catalyst  
15 from the catalyst hopper (6) and / or a catalyst  
16 recovery system (4) are introduced into a holding tank  
17 (5). The contaminated equipment or product is placed  
18 in the decontamination trays (10) and the trays (10)  
19 are lowered into the treatment chamber (1). The lid is  
20 closed and interlocks engaged before the process is  
21 allowed to start. In order to maintain the catalyst in  
22 suspension within the medium, the medium is circulated  
23 by means of a circulation pump (3) and a medium  
24 distribution system (11) having a plurality of rotating  
25 spray heads (not shown). The distribution system (11)  
26 creates a pressure jet effect that develops a catalyst  
27 laden mist or aerosol within the treatment chamber (1)  
28 which facilitates optimum contact / interaction between  
29 the UV light, catalyst and target material on the

1 contaminated instruments. The carrier medium drains to  
2 the bottom of the treatment chamber (1) where it is  
3 collected in a circulation header tank (12) which in  
4 turn feeds the circulation pump (3). At the end of the  
5 treatment process any excess catalyst is recovered from  
6 the medium via a catalyst recovery system (4). As  
7 described above, a process control (not shown) is  
8 provided to monitor progress of the treatment by means  
9 of off-gas monitor / treatment system (8). Upon  
10 completion of the treatment process, the lid is  
11 removed, trays raised and the decontaminated  
12 instruments removed.

13  
14 The medium, including suspended catalyst, may be  
15 circulated directly through the treatment chamber (1)  
16 from the holding tank (5) during the decontamination  
17 process or via the catalyst treatment unit (4) during  
18 the catalyst recovery cycle. Carrier medium is sampled  
19 for conformity / quality maintenance as described in  
20 relation to the previous embodiment. The medium level  
21 within the circulation header tank (12) is monitored  
22 prior to and during operation and is topped-up as  
23 required.

24  
25 The third embodiment, shown schematically in Figure 3  
26 with details of the treatment chamber arrangement shown  
27 in Figures 4 and 5, is designed for either high or low  
28 volume destruction of high level bio-hazards such as  
29 chemical or biological agent materials, prion

1 contaminated material or the like (and may be adapted  
2 to handle solid, liquid or gas phase hazardous  
3 materials). It is envisaged that such a system would  
4 be operated in a restricted area by dedicated and  
5 suitably trained staff.  
6  
7 The apparatus comprises a series treatment chambers (1)  
8 the number and configuration of which may be adapted  
9 depending upon the nature and quantity of material to  
10 be treated. The target material in a suitable pre-  
11 prepared state is introduced from a target material  
12 hopper (13) under control of metering means (14) into a  
13 mixing vessel (15). The carrier medium is fed in to  
14 the mixing vessel (15) from the circulation header tank  
15 (12) by the circulation pump (3) and catalyst is added  
16 from a catalyst hopper (6). The pre-treatment  
17 preparation of the target material may include but need  
18 not be limited to the breaking down of solids into  
19 smaller particles, the suspension of solid particles in  
20 a liquid or the absorption of a gas into a liquid. The  
21 target material, medium and catalyst mixture cascades  
22 into distribution header (16) from which it enters the  
23 treatment chambers (1). This method of controlling the  
24 flow of the mixture removes any potential pressure  
25 other than the hydrostatic head determined by the  
26 relationship between the mixing vessel (15) and the  
27 distribution header (16). Each treatment chamber (1)  
28 comprises a housing that contains a series of tray-like  
29 treatment beds and a light source (2). The treatments

1 beds are designed to maximise the time which the  
2 carrier medium, catalyst and target material mixture is  
3 exposed to the UV light, as well as promoting the  
4 formation of turbulent flow. Typically each treatment  
5 bed comprises of a series of channels (17) running back  
6 and forth across the bed, each channel (17) containing  
7 a textured surface (18) designed to induce turbulent  
8 flow within the mixture. Control of the flow in this  
9 manner prevents the catalyst and target material from  
10 being shielded (as could occur in a laminar flow  
11 situation) and maximises irradiation effectiveness.  
12 The treatment beds are configured with a light source  
13 (2), optionally shrouded with a mirror, directly  
14 overhead. Each treatment bed further comprises a  
15 transparent top plate, typically made from quartz or  
16 some other material having suitable light transmission  
17 characteristics. The treatment mixture is circulated  
18 around the system until the process has been completed  
19 or for a suitable duration as dictated by the operator.  
20 Any suspended solids, catalyst and other waste products  
21 are removed via a catalyst / waste treatment system (4)  
22 for storage prior to final disposal.  
23  
24 Specific modifications may be introduced into the  
25 carrier medium composition and flow control in order to  
26 create the necessary environment for the target  
27 material to be suspended within the medium. For  
28 example, rotary, ultrasonic or other stirring /

25

1 agitation means make be incorporated into the  
2 apparatus.

3

4 The process is controlled using a suitable process  
5 monitoring and control system. This includes  
6 monitoring the off-gas status by means of an off-gas  
7 monitoring / treatment system (8). The off-gas  
8 monitoring / treatment system (8) also provides a means  
9 for the monitoring and collection / treatment of  
10 gaseous reaction products such CO<sub>2</sub>, NO<sub>x</sub>, SO<sub>x</sub> and the  
11 like. In order to treat these off-gases specific  
12 equipment such as scrubbers and absorbers may be  
13 provided. As before suitable analytical techniques can  
14 be employed to monitor the course of the treatment and  
15 the content of used waste products and used carrier  
16 medium.

17

18 The invention is not limited to the embodiments herein  
19 described which can be varied in construction and  
20 detail.

21

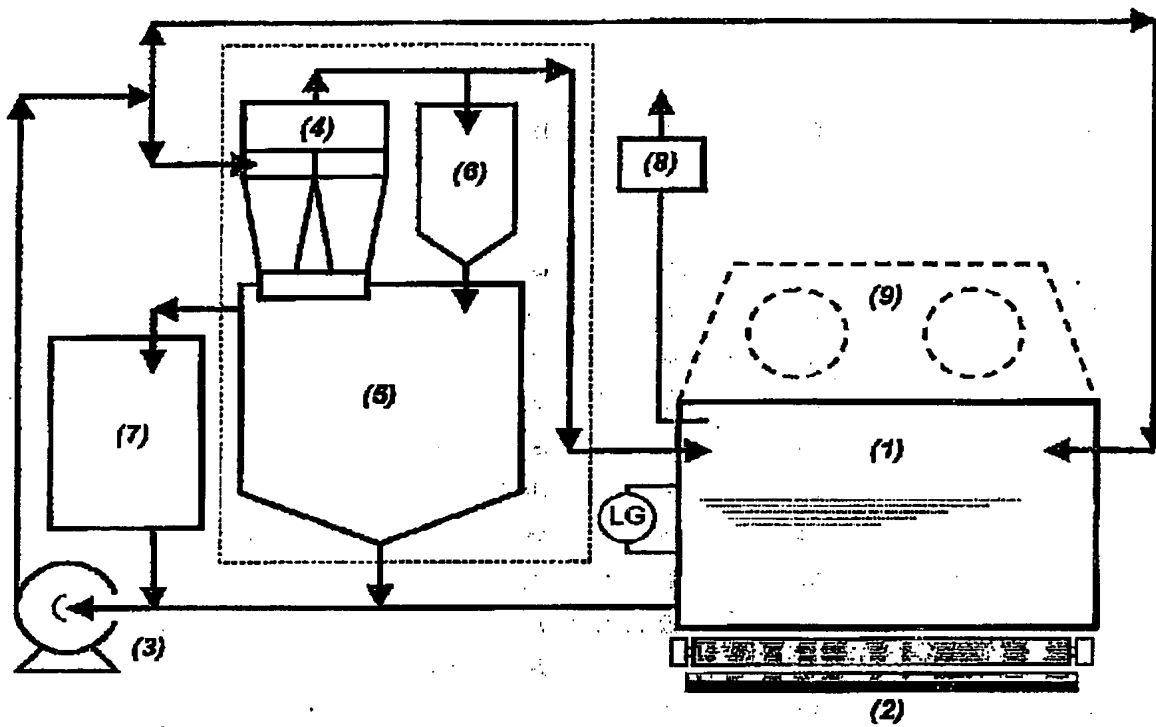
26

1 METHOD FOR THE DEACTIVATION OF CHEMICAL AND BIOLOGICAL  
2 HAZARDS.

3

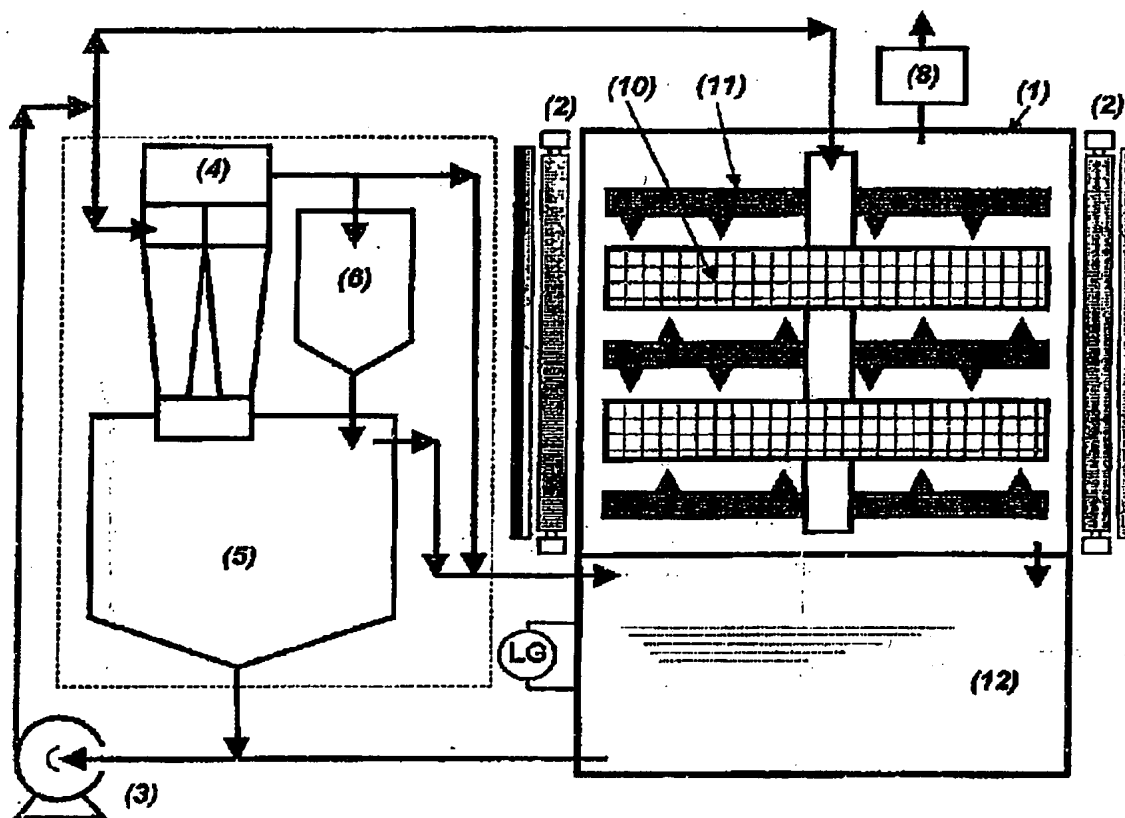
4 The present invention relates to a method for the  
5 deactivation and / or destruction of hazardous  
6 materials such as chemical or biological agents. The  
7 invention further relates to apparatus for treating  
8 hazardous material and for decontaminating items that  
9 may have come into contact with it, the apparatus  
10 comprising a treatment vessel or chamber and a light  
11 source capable of irradiating a catalyst within the  
12 treatment vessel or chamber with a predetermined  
13 wavelength of light.

1 of 4

**Figure 1**

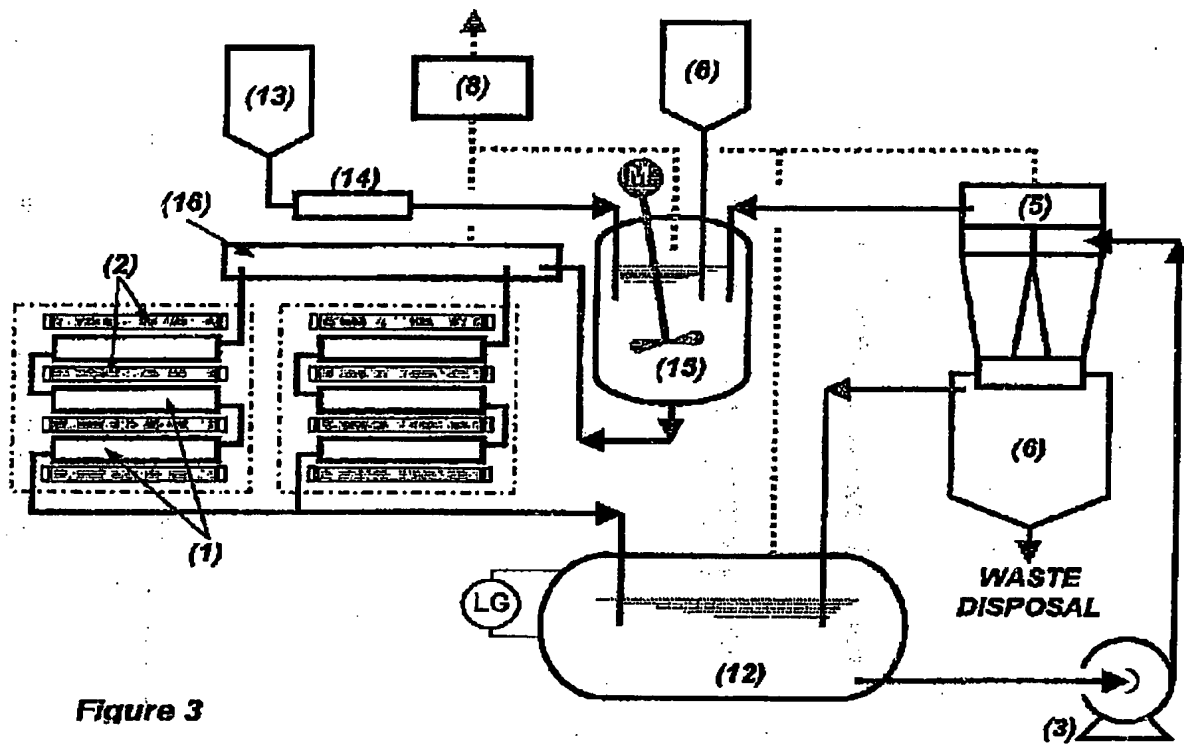


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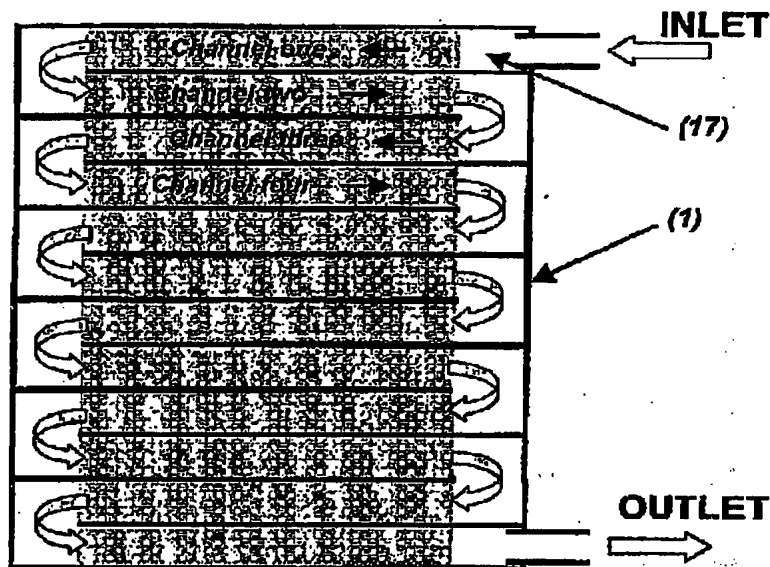
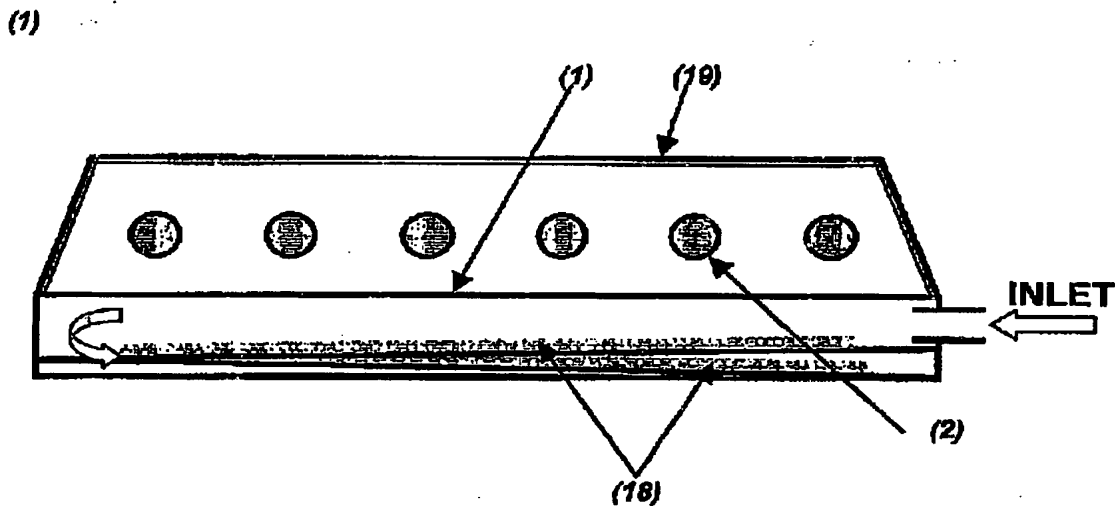


**Figure 2**

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**Figure 3**

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**Figure 4****Figure 5**